

HW 1 KEY

CH 2

D 1.3

$$z = \frac{PV_m}{RT}$$

$$z = \frac{V_{\text{actual}}}{V_{\text{ideal}}}$$

As pressure increases, $z > 1$, molecules are colliding more often, intermolecular repulsive forces dominate, and $V_{\text{real gas}} > V_{\text{ideal gas}}$.
At low pressures, $z \approx 1$ and gases tend to exhibit ideal behavior, no intermolecular forces. At intermediate pressures, $z < 1$ because attractive forces will dominate and $V_{\text{real}} < V_{\text{ideal}}$.

E 1.2 a) $P_1 V_1 = P_2 V_2$

$$V_2 = 4.65 \text{ dm}^3$$

$$P_2 = 5.04 \text{ bar}$$

$$P_1 = \frac{4.65 \text{ dm}^3}{6.85 \text{ dm}^3} (5.04 \text{ bar})$$

$$V_1 = (4.65 + 2.20) \text{ dm}^3$$

$$P_1 = 3.42 \text{ bar}$$

$$P_1 = \frac{3.42 \text{ bar}}{1.013 \text{ bar}} = 3.38 \text{ atm}$$

E 1.13 a

$$a) P = \frac{nRT}{V}$$

$$n = 1, T = 273.15 \text{ K (i) or } 1000 \text{ K (ii)}$$

$$V = 22.414 \text{ dm}^3 \text{ (i) or } 100 \text{ cm}^3 \text{ (ii)}$$

Remember, $\text{dm}^3 = \text{L}$

$$P = \frac{(1 \text{ mol}) (0.08206 \text{ Latm K}^{-1} \text{ mol}^{-1}) (273.15 \text{ K})}{22.414 \text{ L}} = 1.0 \text{ atm : i}$$

Same work for ii: $P = 820 \text{ atm}$

$$\text{Since } 100 \text{ cm}^3 = 0.100 \text{ dm}^3 = 0.100 \text{ L}$$

E 1.18 a

Dalton's Law of Partial Pressures

$$a) n_{\text{total}} = n_{\text{H}_2} + n_{\text{N}_2} = 3 \text{ mol}$$

$$n_{\text{H}_2} = 2 \text{ mol} \quad n_{\text{N}_2} = 1 \text{ mol}$$

$$X_{\text{H}_2} = \frac{2 \text{ mol}}{3 \text{ mol}} = 0.667 \quad X_{\text{N}_2} = 0.333$$

$$b) P_i = X_i P_{\text{total}}$$

$$P_{\text{total}} = \frac{n_{\text{total}} RT}{V}$$

=> Ideal gas law holds
for individual component
gases

$$P_{\text{H}_2} = \frac{2 \text{ mol} (0.08206 \text{ Latm K}^{-1} \text{ mol}^{-1}) (273.15 \text{ K})}{22.4 \text{ L}}$$

$$P_{\text{H}_2} = 2.0 \text{ atm}$$

$$P_{\text{N}_2} = \frac{P_{\text{H}_2}}{2} = 1 \text{ atm}$$

$$c) P_{\text{total}} = \sum_i P_i = P_{\text{H}_2} + P_{\text{N}_2} = 3 \text{ atm}$$

E 1.22 a

Solve VDW equation for b:

$$b = V_m - \frac{RT}{\left(P + \frac{a}{V_m^2} \right)} = \frac{5 \times 10^{-4} \text{ m}^3}{\text{mol}} - \frac{8.314 \text{ J K}^{-1} \text{ mol}^{-1} \cdot 273 \text{ K}}{\left[3 \times 10^6 \text{ Pa} + \left(\frac{0.5 \text{ m}^6 \text{ Pa mol}^{-2}}{(5 \times 10^{-4} \text{ m}^3 \text{ mol}^{-1})^2} \right) \right]}$$

$$b = 0.46 \times 10^{-4} \text{ m}^3 \text{ mol}^{-1}$$

E1.22a cont.

$$Z = \frac{PV}{nRT} = \frac{PV_m}{RT} = \frac{(3 \times 10^6 \text{ Pa})(5 \times 10^{-4} \text{ m}^3)}{(8.314 \text{ J K}^{-1} \text{ mol}^{-1})(273 \text{ K})} = 0.66$$

N1.23 $T = 298 \text{ K}$ $P = 1 \text{ atm}$

$$\frac{2.2990 \text{ g}}{28.02 \text{ g}} \Big| \frac{1 \text{ mol N}_2}{28.02 \text{ g}} = 0.08205 \text{ mol N}_2$$

Mixture: $(2.3102 - 2.2990) \text{ g} = 0.0112 \text{ g Ar}$

$$\frac{0.0112 \text{ g Ar}}{37.95 \text{ g}} \Big| \frac{1 \text{ mol Ar}}{37.95 \text{ g}} = 2.8 \times 10^{-4} \text{ mol Ar}$$

$$X_{\text{Ar}} = \frac{2.8 \times 10^{-4} \text{ mol Ar}}{(2.8 \times 10^{-4} + 0.08205) \text{ mol total}} = \del{0.003} 0.003$$

CH2

D2.3

$\Delta U = q + w$ (heat + work), and the total energy change of the system. Enthalpy is heat transfer, and $\Delta H = \Delta U + p\Delta V$, which is heat transfer at constant pressure, p (thus, $\Delta H = q_p$).

E2.2a

Expansion against constant pressure

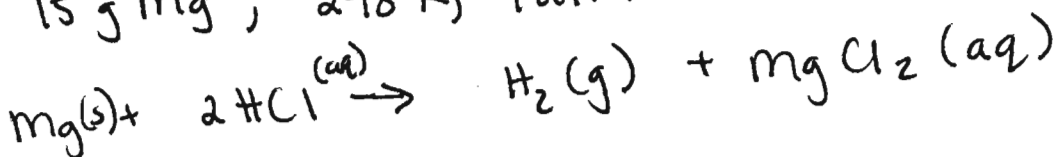
$$w = -P_{\text{ext}} \Delta V \quad P_{\text{ext}} = 1 \text{ atm} \left(\frac{1.01 \times 10^5 \text{ Pa}}{1 \text{ atm}} \right) = 1.01 \times 10^5 \text{ Pa}$$

$$\Delta V = 100 \text{ cm}^2 (10 \text{ cm}) = \frac{1000 \text{ cm}^3}{\left(\frac{10^{-2}}{\text{cm}}\right)^3} = 10^{-3} \text{ m}^3$$

$$w = -(1.01 \times 10^5 \text{ Pa})(10^{-3} \text{ m}^3) = \boxed{-101 \text{ J} = w}$$

E2.7a

15 g Mg, 298 K, 1 atm



$$V_i(\text{H}_2) = 0$$

$$V_f = \frac{n(\text{H}_2)RT}{P} = \frac{\left(\frac{15 \text{ g}}{24.312} \right) \left(\frac{1 \text{ mol H}_2}{1 \text{ mol Mg}} \right) \left(\frac{0.08206 \text{ Latm}}{\text{K mol}} \right) (298 \text{ K})}{1 \text{ atm}}$$

$$V_f = \text{~~15.08~~ 15.08 L}$$

$$w = -P_{\text{ext}} \Delta V = -1 \text{ atm} (9.57 - 0) L = -9.57 \text{ Latm} \left(\frac{101.3 \text{ J}}{1 \text{ atm L}} \right) = \text{~~-1520 J~~ -970 J}$$

Sorry, poor use of calculator: $w = -7.5 \text{ kJ}$

E2.16a

$\Delta H^\circ_{\text{vap}} = 26.0 \text{ kJ/mol}$, 0.50 mol , $T = 250 \text{ K}$, $P = 750 \text{ torr}$

want: $q, w, \Delta H, \Delta U$

Constant pressure:

$q_P = \Delta H = n \Delta H^\circ_{\text{vap}} T_f = (0.50 \text{ mol})(26 \text{ kJ/mol})(250 \text{ K})$

$q_P = 13.0 \text{ kJ} = \Delta H$

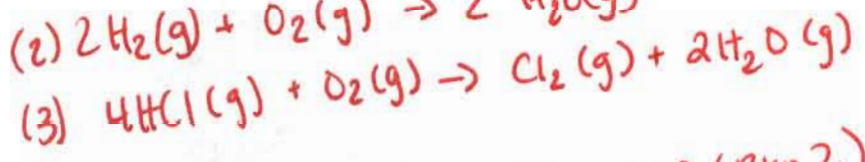
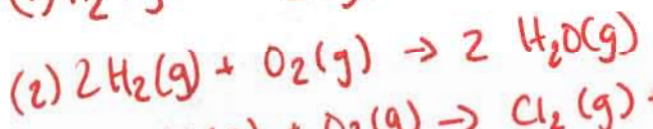
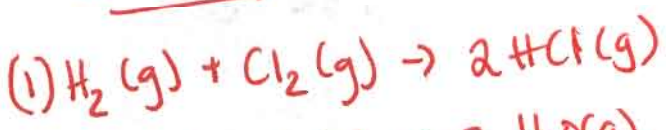
$w = -P_{\text{ext}} \Delta V = -P_{\text{ext}} V_f = -nRT = -(0.50 \text{ mol})(8.314 \text{ J/mol K})(250 \text{ K})$

$w = -1.0 \text{ kJ}$

$\Delta U = q + w = 13 \text{ kJ} - 1 \text{ kJ} = 12 \text{ kJ}$

~~E2.22a~~

E 2.22a



$\Delta_r H^\circ = -2 \Delta_r H^\circ(\text{Rxn 1}) + \Delta_r H^\circ(\text{Rxn 2}) = -2(-184.62) + (-483.64) = -114.4 \frac{\text{kJ}}{\text{mol}}$

$\Delta_r U^\circ = \Delta_r H^\circ - \Delta n_g RT = (-114.4 \text{ kJ/mol}) - (-1)(298 \text{ K})(8.314 \text{ J/mol K})$

$\Delta n_g = -1$ $\Delta_r U^\circ = -111.92 \text{ kJ/mol}$

b) $\Delta_f H(\text{molecule}) = \frac{\Delta_r H^\circ(\text{molecule})}{\nu_{\text{molecule}}}$

$\Delta_f H(\text{HCl}(\text{g})) = \frac{-184.62 \text{ kJ mol}^{-1}}{2} = -92.31 \text{ kJ mol}^{-1}$

$\Delta_f H(\text{H}_2\text{O}(\text{g})) = \frac{-483.64}{2} = -241.82 \text{ kJ mol}^{-1}$



$SO_4^{2-} \rightarrow$ spectator ion

$$\Delta_r H^\circ = \sum_{\text{prod}} \nu_i H_i^\circ - \sum_{\text{react.}} \nu_i H_i^\circ = -218.66 \text{ kJ/mol}$$

N 2.1

1) $T_1 = \frac{PV_1}{nR} = \frac{(1 \text{ atm})(22.44 \text{ L})}{0.08206 \text{ LatmK}^{-1}\text{mol}^{-1}} = 273.46 \text{ K} = T_1$

2) Same way, $T_2 = 2T_1 = 546.92 \text{ K} = T_2$

3) $P_3 = \frac{1}{2} P_1, V_3 = 2V_1, T_3 = T_1 = 273.46 \text{ K}$ (along isotherm)

Let's consider all steps to be reversible:

Step 1-2 $w = -P_{\text{ext}} \Delta V = -nR \Delta T = (-1 \text{ mol})(8.314 \text{ J K}^{-1}\text{mol}^{-1})(273 \text{ K}) = -2.27 \text{ kJ}$

$$\Delta U = n C_{v,m} \Delta T = (1 \text{ mol})\left(\frac{3}{2} R\right)(273 \text{ K}) = 3.4 \text{ kJ}$$

$$q = \Delta U - w = 3.40 \text{ kJ} - (-2.27 \text{ kJ}) = 5.67 \times 10^3 \text{ J}$$

$$\Delta H = q_p = 5.67 \text{ kJ}$$

Step 2 \rightarrow 3 Constant $V, w = 0$

$$q_v = \Delta U = n C_{v,m} \Delta T = (1 \text{ mol})\left(\frac{3}{2} R\right)(-273 \text{ K}) = -3.40 \text{ kJ}$$

ALSO: $\Delta U_{\text{tot}} = 0$, so $\Delta U_1 = -\Delta U_2$, since $\Delta U_3 = 0$ (isotherm)

Since $\Delta H \equiv \Delta U + \Delta(PV) = \Delta U + \Delta(nRT) = \Delta U + nR \Delta T$

Here, $\Delta T = -273, \Delta H = -5.67 \times 10^3 \text{ J} = -5.67 \text{ kJ}$

Step 3 \rightarrow 1 $\Delta U = 0 = \Delta H$, along isothermal process in I.G.

$$-q = w = -nRT \ln \frac{V_1}{V_3} = -(1 \text{ mol})(8.314)(273 \text{ K}) \ln\left(\frac{1}{2}\right)$$

$$-q = 1.57 \text{ kJ} \quad q = -1.57 \text{ kJ}$$

	$q(\text{kJ})$	$w(\text{kJ})$	ΔU	ΔH
Step 1 \rightarrow 2	5.67	-2.27	3.40	5.67
2 \rightarrow 3	-3.40	0	-3.40	-5.67
3 \rightarrow 1	-1.57	1.57	0	0
cycle	0.70	-0.70	0	0

DR. VDB's problems:

1) $8.314 \text{ J K}^{-1} \text{ mol}^{-1}$, $\bar{V} = \text{Pa m}^3$, $1 \text{ Pa} = 10^{-6} \text{ MPa}$

$$\frac{8.314 \text{ m}^3 \text{ Pa}}{\text{mol K}} \left| \frac{10^{-6} \text{ cm}^3}{\text{m}^3} \right| \frac{\text{MPa}}{10^6 \text{ Pa}} = \frac{8.314 \text{ cm}^3 \text{ MPa}}{\text{mol K}}$$

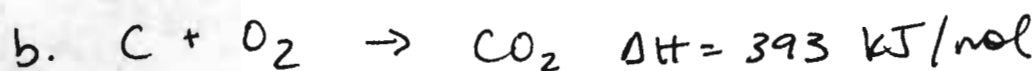
$$1 \text{ cm}^3 = 1 \text{ mL} = 2.6 \times 10^{-4} \text{ gallons}$$

$$14.5 \text{ bar} = 1 \text{ psi}$$

$$\frac{8.314 \text{ cm}^3 \text{ MPa}}{\text{mol K}} \left| \frac{1 \text{ mL}}{\text{cm}^3} \right| \frac{2.6 \times 10^{-4} \text{ gal}}{1 \text{ mL}} \left| \frac{1 \text{ psi}}{14.5 \text{ MPa}} \right| = \frac{1.5 \times 10^{-5} \text{ gal} \cdot \text{psi}}{\text{mol} \cdot \text{K}} = R$$

2) a. ΔV (potential energy) = mgh

$$= (50 \text{ kg})(9.8 \text{ m s}^{-2})(1 \text{ m}) = 490 \text{ kg m}^2 \text{ s}^{-2} = 490 \text{ J}$$



$$\frac{1 \text{ g C}}{12 \text{ g C}} \left| \frac{1 \text{ mol C}}{1 \text{ mol C}} \right| \frac{393 \text{ kJ}}{1 \text{ mol C}} = 3.28 \times 10^4 \text{ J} \quad (k = 10^3)$$

$$\text{c. } \frac{1840 \text{ kcal}}{k} \left| \frac{10^3}{k} \right| \frac{4.184 \text{ J}}{1 \text{ cal}} = 7.7 \times 10^6 \text{ J}$$

$$\text{d. } 100 \text{ W} = \frac{100 \text{ J}}{\text{s}} \left| \frac{3600 \text{ s}}{1 \text{ hr}} \right| \frac{24 \text{ hr}}{1 \text{ day}} = 8.64 \times 10^6 \text{ J/day}$$

3) $C_{v,m} = 1.5R$ $P_2 = 100 \text{ bar}$ $P_1 = 10 \text{ bar}$ $T = 300 \text{ K}$ $n = 2$

Constant T, ~~$P_1 = 100$~~ , $P_2 = 10 \text{ bar}$

$$\Delta U = q + w$$

Find ΔU , w , q , and what if reversibly

$$w = - \int_{V_i}^{V_f} P dV \quad PV = nRT \quad \text{SO } V_f = \frac{n_f RT}{P_f} \rightarrow \text{same expression for initial volume}$$

$$w = -P_f \Delta V = -P_f \left(\frac{n_f RT}{P_f} - \frac{n_i RT}{P_i} \right) = - \left(nRT - \frac{nRT P_i}{P_f} \right) \quad n_i = n_f$$

$$w = -nRT \left(1 - \frac{P_f}{P_i} \right) = 2 \text{ mol} \cdot 8.314 \text{ J K}^{-1} \text{ mol}^{-1} \cdot 300 \text{ K} \left(1 - \frac{100 \text{ bar}}{10 \text{ bar}} \right) = 4.48 \times 10^4 \text{ J} = w$$

3) continued

Found work, $w = 4.48 \times 10^4 \text{ J}$

$$\Delta U = 0 = q + w, \text{ so } q = -w = -4.48 \times 10^4 \text{ J}$$

Internal energy, U , is a state function, $\Delta U = U_f - U_i$ and $U_f = U_i$
cyclic process $\Delta U = C\Delta T, \Delta T = 0$

Reversible process:

isothermal

$$w = -nRT \ln\left(\frac{V_f}{V_i}\right) \text{ if ideal, } w = -nRT \ln\left(\frac{P_i}{P_f}\right)$$

Step 1:

just care about ratio

~~$w_1 = -nRT \ln\left(\frac{10}{100}\right)$~~

$$w_1 = -nRT \ln\left(\frac{10}{100}\right)$$

Step 2:

$$w_2 = -nRT \ln\left(\frac{100}{10}\right)$$

$$\text{overall, } w_{\text{tot}} = w_1 + w_2 = -nRT \ln\left(\frac{10}{100}\right) + nRT \ln\left(\frac{10}{100}\right) = 0$$

OR: $w_{\text{tot}} = -nRT \ln\left(\frac{P_i}{P_f}\right)$, $P_i = P_f \Rightarrow 0 = w_{\text{tot}}$

$$\Delta U = 0 = q + w = q + 0$$

$$\therefore q = w = 0$$

$$4. w = - \int_{V_1}^{V_2} P dV = - \int \frac{RT}{V_m - b} - \frac{a}{TV_m^2} dV_m$$

$$= - \left[RT \ln(V_m - b) \Big|_{V_1}^{V_2} + \frac{a}{TV_m} \Big|_{V_1}^{V_2} \right]$$

$$= - \left[RT [\ln(V_2 - b) - \ln(V_1 - b)] + \frac{a}{T} \left[\frac{1}{V_2} - \frac{1}{V_1} \right] \right]$$

where $R = 0.08314 \text{ L bar K}^{-1} \text{ mol}^{-1}$, $T = 300 \text{ K}$, $V_2 = \frac{10 \text{ L}}{22.4}$, $V_1 = \frac{4 \text{ L}}{22.4 \text{ L mol}^{-1}}$
 $a = 1080 \text{ L}^2 \text{ mol}^{-1}$ $b = 0.04287 \text{ L mol}^{-1}$

$$w = -40.6 \text{ L bar/mol} = -4060 \text{ J/mol}$$

For isothermal, reversible expansion, ideal gas, $w = -q$, $\Delta U = 0$

$$5. C_p = C_v + T \left(\frac{\partial P}{\partial T} \right)_V \left(\frac{\partial V}{\partial T} \right)_P$$

$$a. P(V - nb) = nRT \quad \therefore P = \frac{nRT}{V - nb}$$

$$V = \frac{nRT}{P} + nb$$

$$\left(\frac{\partial P}{\partial T} \right)_V = \frac{nR}{V - nb} \quad \text{and} \quad \left(\frac{\partial V}{\partial T} \right)_P = \frac{nR}{P}$$

$$C_p = C_v + T \left(\frac{nR}{V - nb} \right) \left(\frac{nR}{P} \right)$$

$$= C_v + \frac{PnR}{P} = \boxed{C_v + nR = C_p}$$



$$\Delta H_f^\circ: \quad 0 \quad -285.83 \quad 0 \quad -240.12 \quad -230 \frac{\text{kJ}}{\text{mol}}$$

$$\Delta H_f^\circ: \\ 350 \text{K}$$

$$\Delta H_{\text{rxn}}^\circ = \sum_{\text{products}} \nu_i \Delta H_i^\circ - \sum_{\text{reactants}} \nu_j \Delta H_j^\circ = [2(-240.12) + (-230)2] - [2(-285.83)] = -368.58 \frac{\text{kJ}}{\text{mol}}$$

$$\Delta H_r(T_2) = \Delta H_r(T_1) + \int_{T_1}^{T_2} \Delta_r C_p^\circ dT, \text{ where } \Delta_r C_p^\circ = \sum_{\text{prod.}} \nu C_{p,m}^\circ - \sum_{\text{reactants}} \nu C_{p,m}^\circ$$

(if C_p° is temperature independent, $\Delta H_r(T_2) = \Delta H_r(T_1) + \Delta_r C_p^\circ \Delta T$)

$$\Delta_r C_{p,m}^\circ = [28.82 + 2(46.4) + 2(-148.5)] - [2(-75.3) + 2(28.24)]$$

All values for STP (thermo) and were found in text appendix, in J/mol

$$\Delta_r C_p^\circ = -81.28 \text{ J/mol}$$

$$\Delta H_r(350 \text{K}) = \Delta H_r(298 \text{K}) + \Delta_r C_p^\circ \Delta T = -368.58 \frac{\text{kJ}}{\text{mol}} + (-81.28 \frac{\text{J}}{\text{mol}})(52 \text{K})$$

$$\Delta H_r(350 \text{K}) = -372.8 \text{ kJ/mol}$$

Work: constant pressure $w = -P_{\text{ext}} \Delta V$

$$L_{\text{atm}} \approx 101 \text{ J} \quad V_i \approx 0, \quad V_f = \frac{nRT}{P_{\text{ext}}} = \frac{\left(\frac{10 \text{g Na}}{23 \text{g}} \mid 1 \text{ mol Na} \mid 1 \text{ mol H}_2(g) \right)}{2 \text{ mol Na}} \left(\frac{0.08206}{\text{atm}} \right) (T)$$

$$V_f(298 \text{K}) = 5.31 \text{ L}; \quad w \approx -531 \text{ J}$$

$$V_f(350 \text{K}) = 6.23 \text{ L}; \quad w \approx -623 \text{ J}$$

$$\text{For } 0.217 \text{ mol H}_2(10 \text{g Na}), \quad \Delta H = -368.58 \text{ kJ/mol} (0.217) = 80 \text{ kJ}$$

magnitude of $\Delta H \gg$ magnitude work